

# Control Volumes

## 1 Conservation of Mass

In the previous chapter we looked at closed systems. Now we look at control volumes. A **control volume** is a fixed volume in space, where mass can move through. Just like we have applied conservation of energy in closed systems, we can apply the **conservation of mass principle** in control volumes. So we have

$$\Delta m = m_{in} - m_{out}. \quad (1.1)$$

The **mass flow rate**  $\dot{m}$  is the mass flowing through a cross-section per unit time. Suppose we have a pipe or duct. We can then determine the mass flow through this pipe using

$$\dot{m} = \int_{A_c} \rho \nu_n dA_c = \rho \nu_{n,avg} A_c, \quad (1.2)$$

where  $A_c$  is the cross-sectional area of the pipe and  $\nu_n$  is the velocity of the flow normal to this area. Identically, we can define the **volume flow rate**  $\dot{V}$  as

$$\dot{V} = \int_{A_c} \nu_n dA_c = \nu_{n,avg} A_c = \dot{m} v. \quad (1.3)$$

We can now rewrite the conservation of mass principle as

$$\frac{dm}{dt} = \dot{m}_{in} - \dot{m}_{out}. \quad (1.4)$$

## 2 Energy of a Flowing Fluid

The interesting thing about a control volume, is that mass can enter it. What we want to know is how much energy is added to the system when a piece of mass enters a control volume. First of all, we know that the specific energy  $e$  consists of specific internal energy  $u$ , specific kinetic energy  $V^2/2$  and specific potential energy  $gz$ . But there is more.

When a mass enters a control volume, something pushes it in. This pushing performs so-called **flow work** (also called **flow energy**), having magnitude

$$W_{flow} = PV, \quad \text{or, expressed per unit mass,} \quad w_{flow} = Pv. \quad (2.1)$$

So we find that the **total energy of a flowing fluid** per unit mass is

$$\theta = w_{flow} + e = Pv + u + \frac{1}{2}V^2 + gz = h + \frac{1}{2}V^2 + gz. \quad (2.2)$$

## 3 Steady Flow Processes

During a **steady flow process** the properties inside the control volume do not change with time. Since the total mass then is constant, we have  $dm/dt = 0$  and thus

$$\dot{m}_{in} = \dot{m}_{out}. \quad (3.1)$$

If the flow is also incompressible, then also

$$\dot{V}_{in} = \dot{V}_{out}. \quad (3.2)$$

For steady flow processes, also the energy stays constant. This implies that  $\dot{E}_{in} = \dot{E}_{out}$ , or equivalently,

$$\dot{Q}_{in} + \dot{W}_{in} + \sum_{in} \dot{m}\theta = \dot{Q}_{out} + \dot{W}_{out} + \sum_{out} \dot{m}\theta. \quad (3.3)$$

If we define  $\dot{Q} = \dot{Q}_{in} - \dot{Q}_{out}$  as the heat that goes into the system and  $\dot{W} = \dot{W}_{out} - \dot{W}_{in}$  as the work done by the system, we will get

$$\dot{Q} - \dot{W} = \dot{m} \left( h_{out} - h_{in} + \frac{V_{out}^2 - V_{in}^2}{2} + g(z_{out} - z_{in}) \right). \quad (3.4)$$

Dividing by  $\dot{m}$  gives

$$q - w = h_{out} - h_{in} + \frac{V_{out}^2 - V_{in}^2}{2} + g(z_{out} - z_{in}), \quad (3.5)$$

where  $q = q_{in} - q_{out}$  and  $w = w_{out} - w_{in}$ .

There are many examples of steady flow devices in real life. For example, a **nozzle** is a device that increases velocity by decreasing the pressure. A **diffuser** does exactly the opposite. For both devices, the amount of heat transferred  $\Delta Q$ , the amount of work performed  $\Delta W$  and the change in potential energy  $\Delta pe$  can be neglected. This reduces the energy balance equation to

$$h_{in} + \frac{1}{2}V_{in}^2 = h_{out} + \frac{1}{2}V_{out}^2. \quad (3.6)$$

A similar thing can be done for other devices with a steady flow processes, such as **turbines** and **compressors**.

## 4 Unsteady Flow Processes

For many processes there are properties inside the control volume that change over time. Such processes are called **unsteady flow processes**. The relations of the previous paragraph are not applicable to those processes.

Dealing with unsteady flow processes is a lot more difficult. We therefore often assume that such processes are uniform flow processes. A **uniform flow process** is a process for which the properties at the inlets and outlets do not change with time or position.

Now let's look at two situations in this flow: One initial situation (1) and one situation a bit later (2). A heat  $Q$  has been added. The system has done an amount of work  $W$ . Also incoming mass has brought an energy  $(m\theta)_{in}$ , and mass leaving the system has taken energy  $(m\theta)_{out}$  with it. Using these data, we can set up the energy balance for uniform flow processes. We get

$$Q - W + (m\theta)_{in} - (m\theta)_{out} = m_2e_2 - m_1e_1. \quad (4.1)$$

Once more this equation can be simplified, based on various assumptions.