

UWE Bristol

Thermodynamics & Fluids

UFMEQU-20-1

FLUIDS

Lecture 2: Turbulent Flow



University of the
West of England

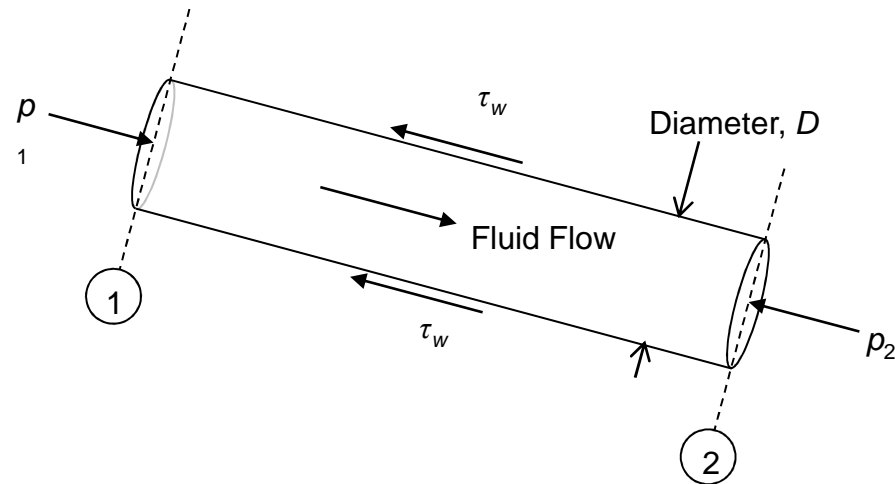
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Today's Lecture

- Last week: Laminar Flow
- This week: Turbulent Flow
- Shear stress
- Pressure drop
- Friction factor
- Determining f (Moody Chart)
- Methods to solve problems

Fluid Flow with Friction

- Same situation:



- Bernoulli's equation:

$$p_1 + \frac{1}{2} \rho C_1^2 + \rho g z_1 = p_2 + \frac{1}{2} \rho C_2^2 + \rho g z_2 + \Delta p$$

$\Delta p = \text{pressure drop}$

- How do we determine Δp ?

Shear Stress

- Experimental results differ from laminar flow
- Dimension analysis to determine relationship

<i>Variable</i>	<i>Description</i>
τ_w	Wall shear stress (the variable we wish to investigate)
ρ	Density
μ	Viscosity
c	Average velocity
D	Pipe diameter (bore)
ε	Pipe roughness

$$\tau_w = \varphi(\rho, \mu, c, D, \varepsilon) \rightarrow \tau_w = K\rho^a \mu^b c^d D^e \varepsilon^f$$

Shear Stress

- Go through dimensional analysis method:

$$\text{MLT}^{-2} = (\text{ML}^{-3})^a (\text{ML}^{-1}\text{T}^{-1})^b (\text{LT}^{-1})^d (\text{L})^e (\text{L})^f$$

Equating powers of each dimension on both sides:

$$\text{For M: } 1 = a + b$$

$$\text{For L: } -1 = -3a - b + d + e + f$$

$$\text{For T: } -2 = -b - d$$

$$a = 1 - b$$

$$d = 2 - b$$

$$e = 3a + b - d - f - 1 = 3(1 - b) + b - (2 - b) - f - 1$$

$$e = -b - f$$

Shear Stress

$$\tau_w = K\rho^a \mu^b c^d D^e \varepsilon^f = K\rho^{1-b} \mu^b c^{2-b} D^{-b-f} \varepsilon^f$$

$$\tau_w = K\rho c^2 \left(\frac{\mu}{\rho c D} \right)^b \left(\frac{\varepsilon}{D} \right)^f$$

- Rearranging:

$$\frac{\tau_w}{\frac{1}{2}\rho c^2} = 2K \left(\frac{\rho c D}{\mu} \right)^{-b} \left(\frac{\varepsilon}{D} \right)^f$$

Non-dimensional wall shear stress

Reynolds Number

Relative Roughness

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Relative Roughness

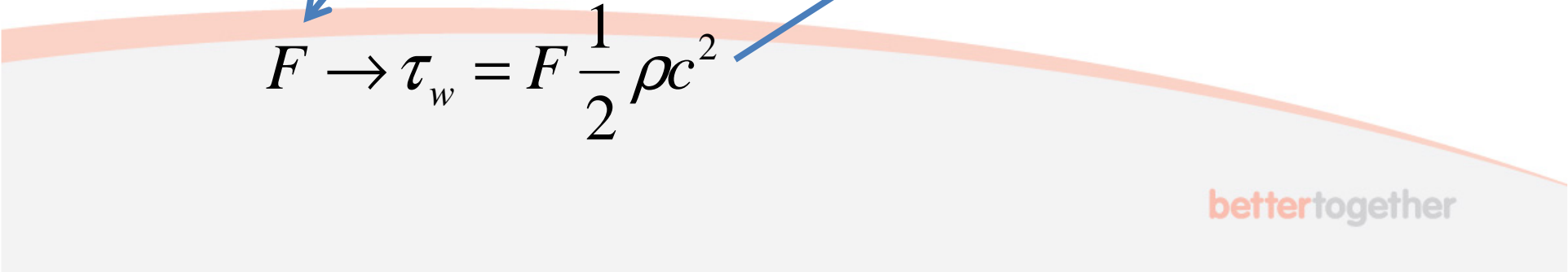
- Measure of how rough pipe wall is
- Measured in metres (or mm)
- Defined by material and manufacture method
- Represented by Epsilon ϵ
- Relative Roughness is ϵ/D
- Non-dimensional (m/m)

Pressure Drop

- Shear stresses are related to
 - Reynolds Number
 - Relative Roughness

$$\frac{\tau_w}{\frac{1}{2}\rho c^2} = F\left(\frac{\rho c D}{\mu}, \frac{\varepsilon}{D}\right)$$

$$\tau_w = \frac{D}{4} \frac{\Delta p}{L} = F \frac{1}{2} \rho c^2$$


$$F \rightarrow \tau_w = F \frac{1}{2} \rho c^2$$

Pressure Drop

- We have:

$$\frac{D}{4} \frac{\Delta p}{L} = F \frac{1}{2} \rho c^2$$

- Rearranging:

$$\Delta p = \frac{4FL}{D} \frac{1}{2} \rho c^2$$

- F is **FANNING FRICTION FACTOR**
- f is **DARCY FRICTION FACTOR = 4F**

Pressure Drop

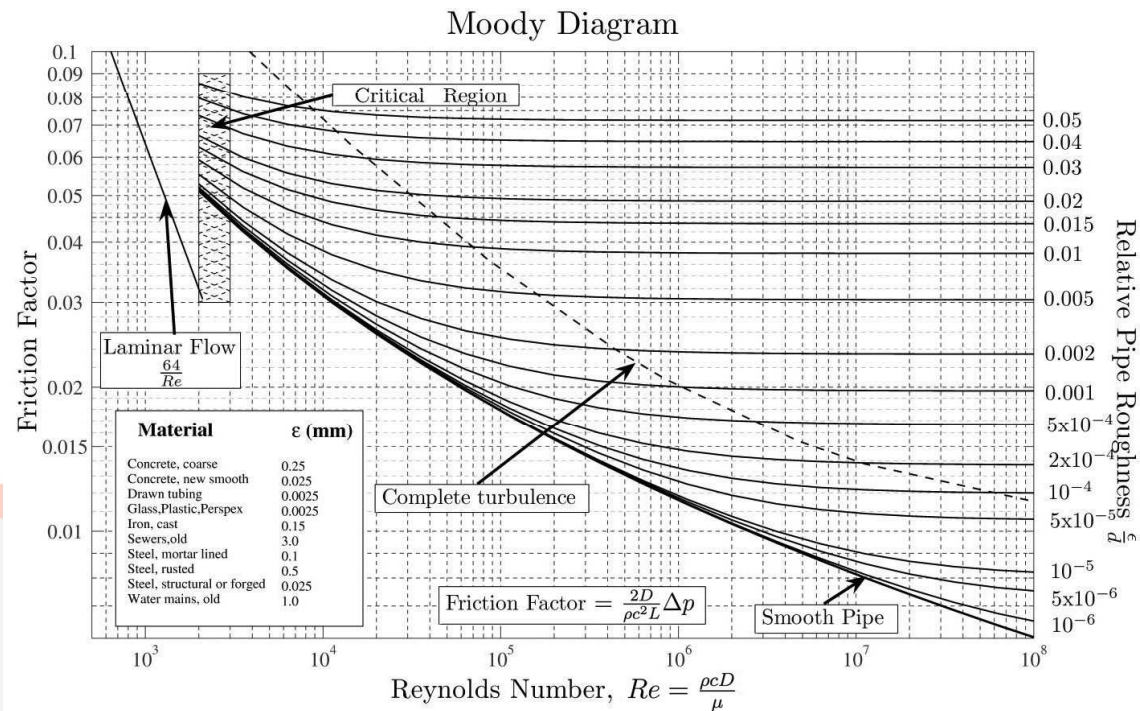
- Replacing Fanning friction factor with Darcy friction factor, f

$$\Delta p = \frac{fL}{D} \frac{1}{2} \rho c^2$$

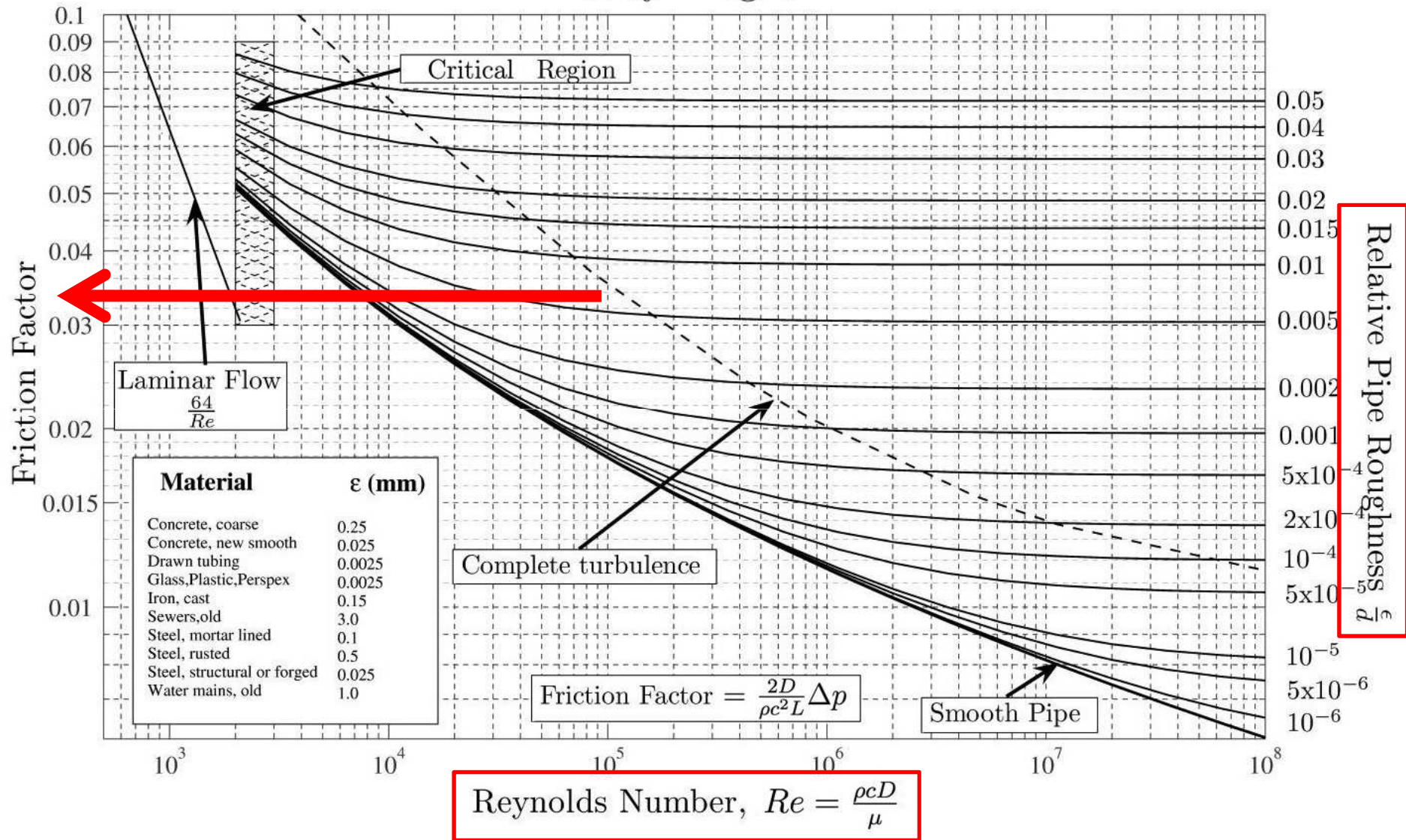
- If we have friction factor, we can calculate pressure drop to insert into Bernoulli's equation.

Friction Factor

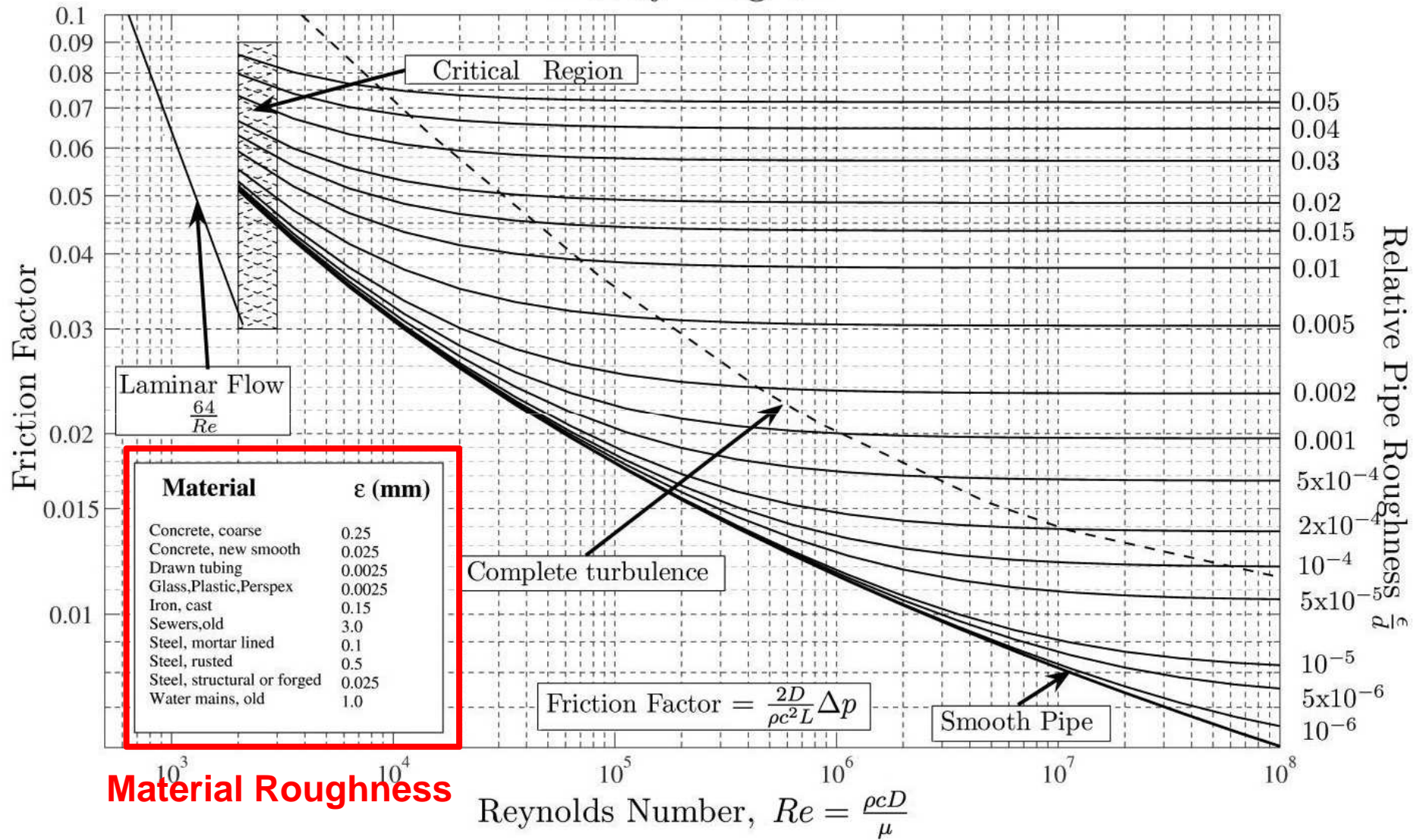
- How do we determine Friction Factor?
- Moody Chart

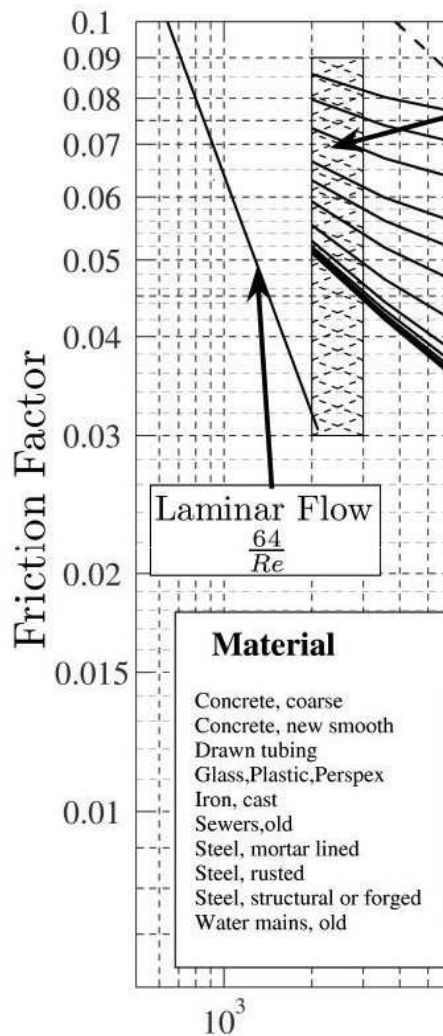


Moody Diagram



Moody Diagram





- Laminar Region ($Re < 2000$)

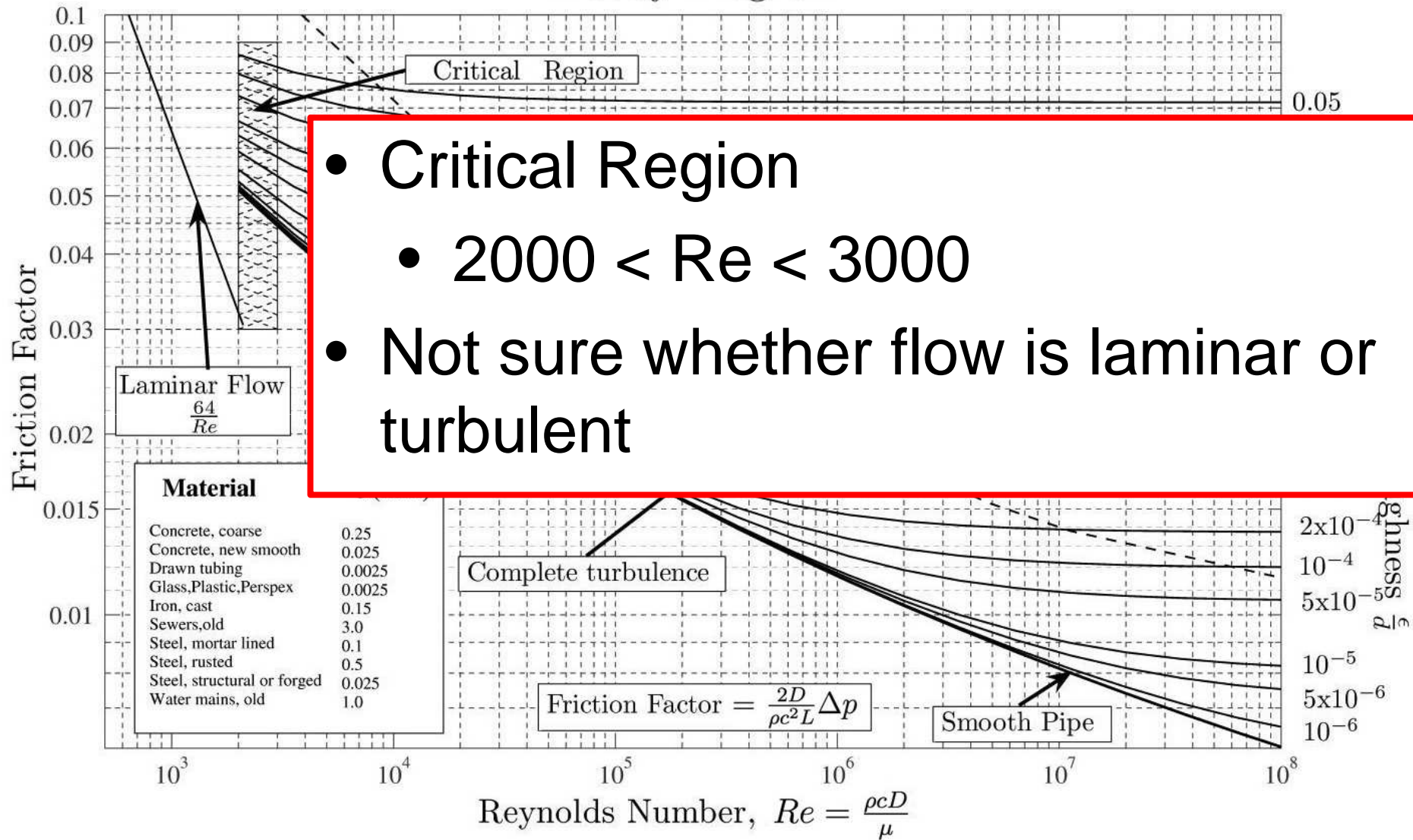
$$\Delta p = \frac{8\mu L \dot{V}}{\pi R^4} = \frac{fL}{D} \frac{1}{2} \rho c^2$$

$$\frac{32\mu Lc}{D^2} = \frac{fL}{D} \frac{1}{2} \rho c^2$$

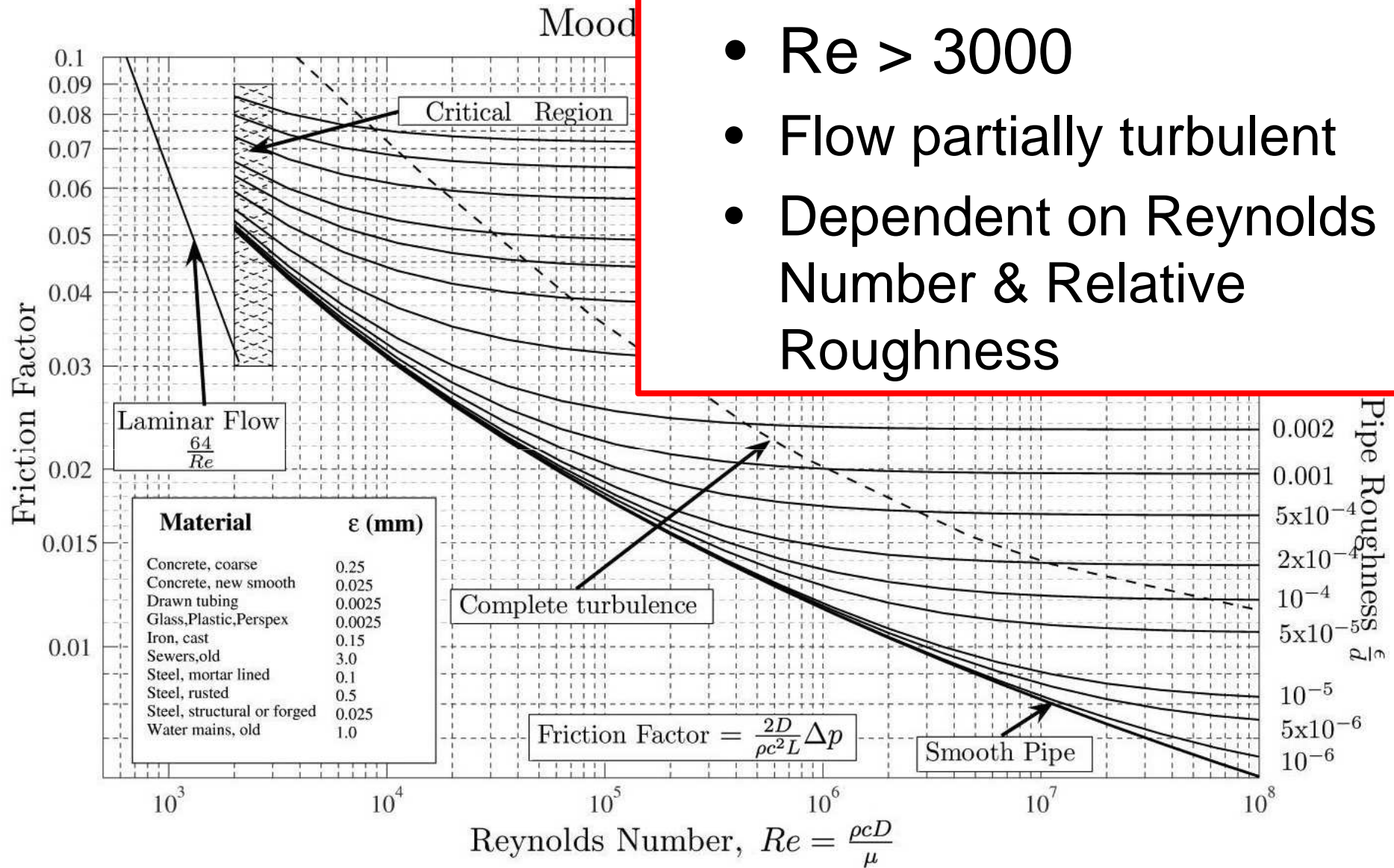
$$f = \frac{64\mu}{\rho c D} = \frac{64}{Re}$$

- So we can use equation from last lecture, or this one!

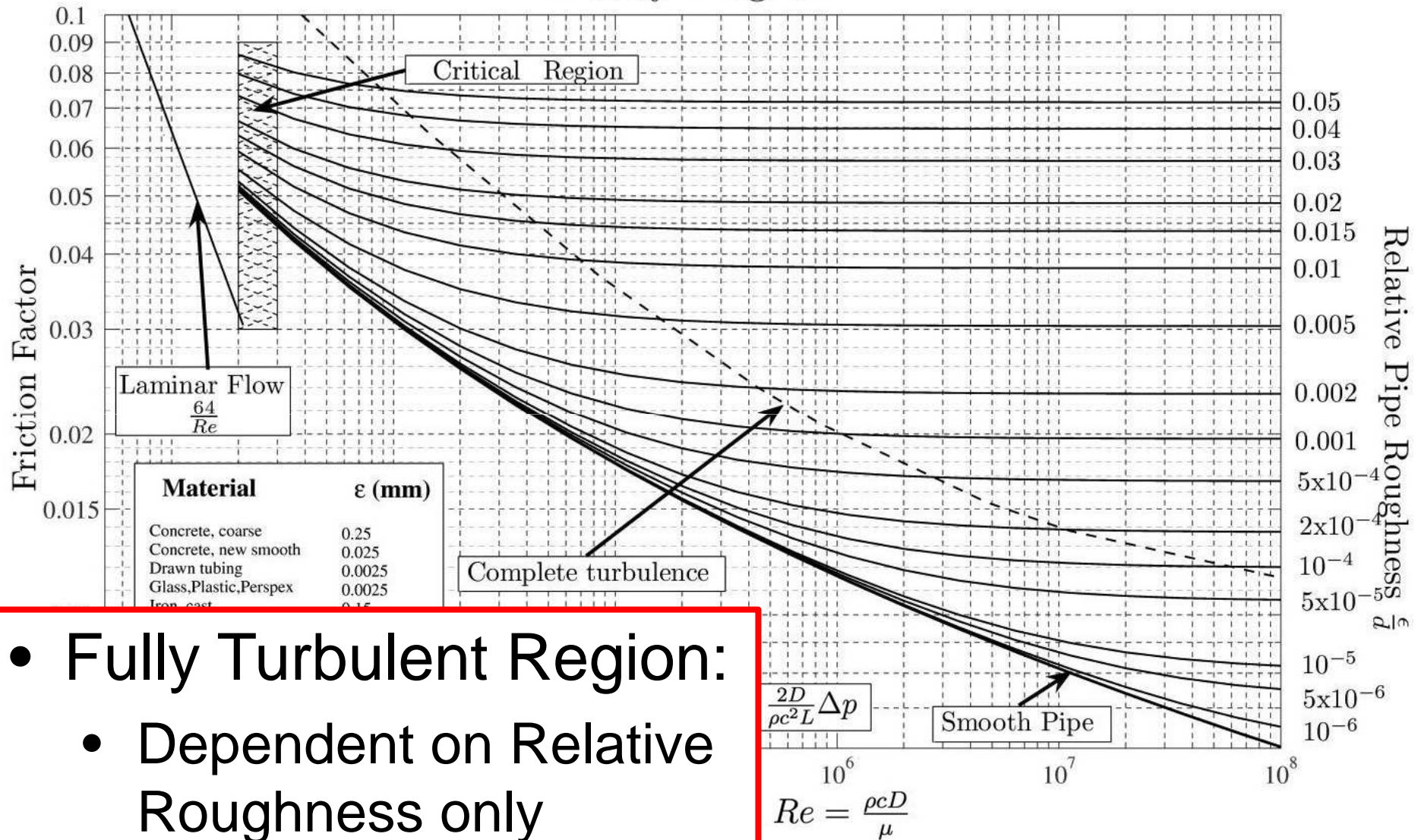
Moody Diagram



- Transition Region
 - $Re > 3000$
 - Flow partially turbulent
 - Dependent on Reynolds Number & Relative Roughness



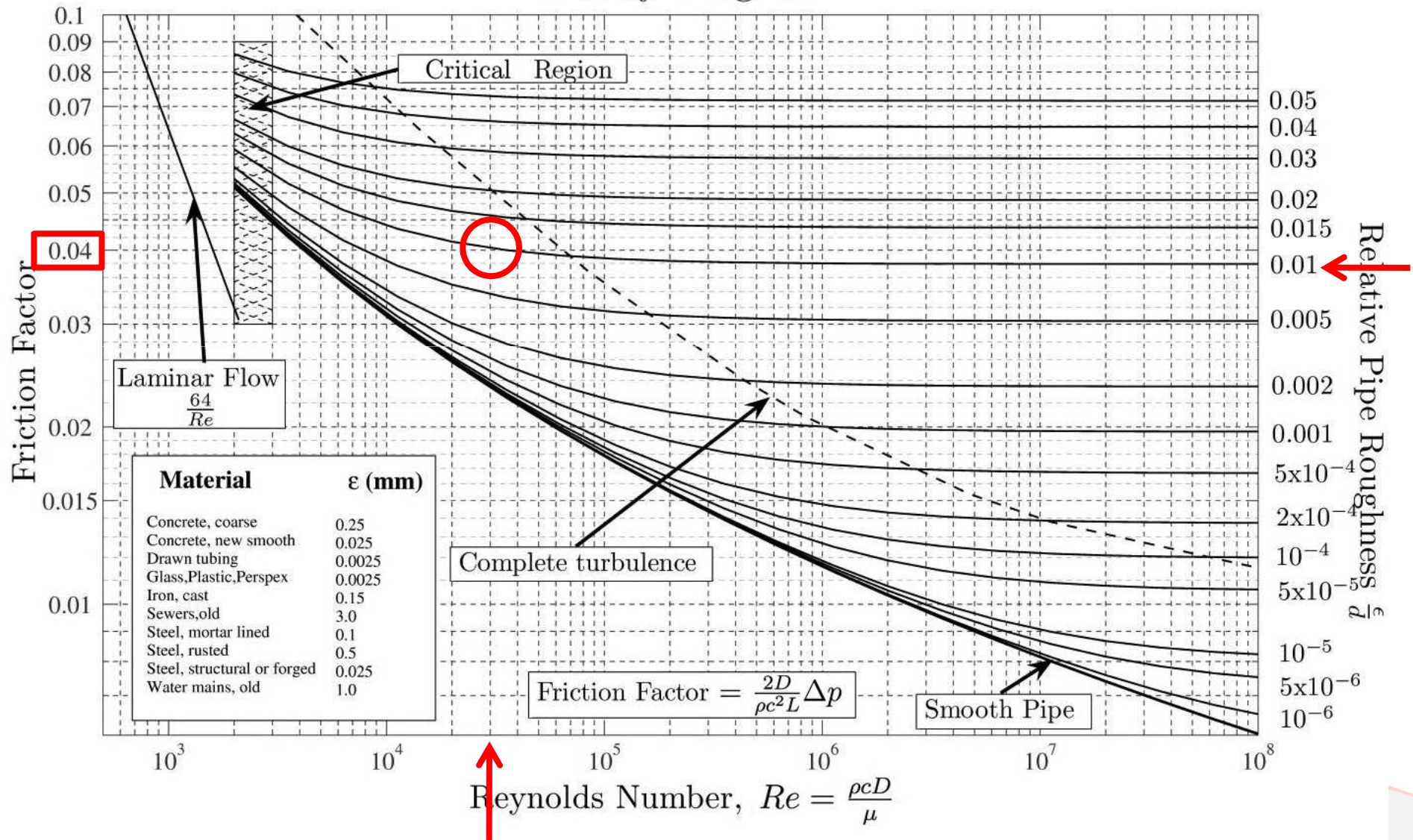
Moody Diagram



- Fully Turbulent Region:
 - Dependent on Relative Roughness only (straight lines)

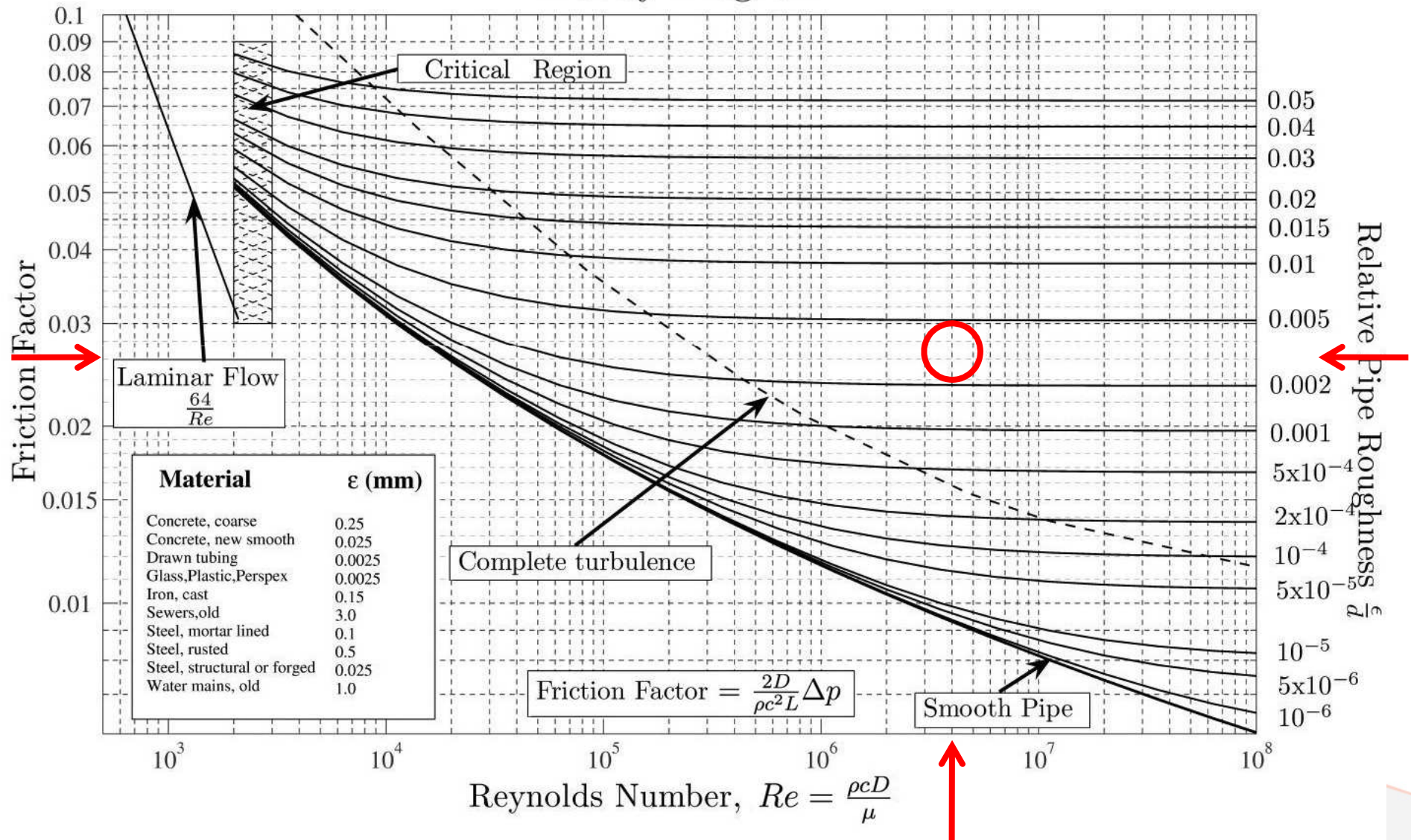
- Example: $Re = 3 \times 10^4$ and $\epsilon/D = 0.01$

Moody Diagram



- Example: $Re = 4 \times 10^6$ and $\epsilon/D = 0.003$

Moody Diagram



Problems

- 3 Types of Problems
 - Type 1 – Pressure drop
 - (Given flow rate and diameter)
 - Know everything so apply equation
 - Type 2 – Flow rate
 - (Given pressure drop and diameter)
 - Don't know c , so cannot find Re !
 - Type 3 – Pipe Diameter
 - (Given pressure drop and flow rate)
 - Don't know D , so cannot find Re or ϵ/D !

Type 1 Problem

- Given:
 - Diameter – use to calculate Reynolds number and relative roughness → Friction factor
- Apply equation to determine Δp

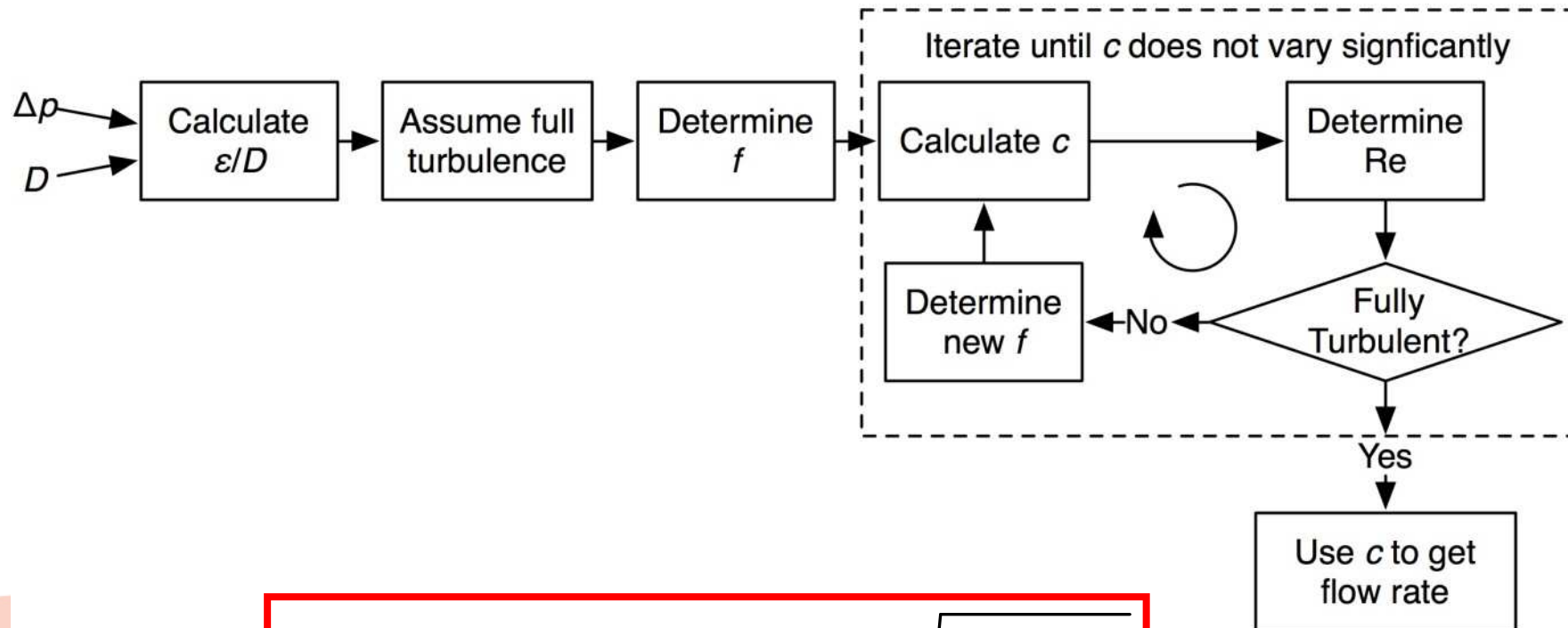
$$\Delta p = \frac{fL}{D} \frac{1}{2} \rho c^2$$

Type 2 Problem

- Given:
 - Δp and Pipe diameter
- Need to find flow rate ($\dot{V} = Ac$)
 - We don't have c , so cannot determine Re
 - How to find f ?
 - Need to assume full turbulence (no need for Reynolds number), then check answer
 - Iteration if necessary

Type 2 Problem

- Flow chart:



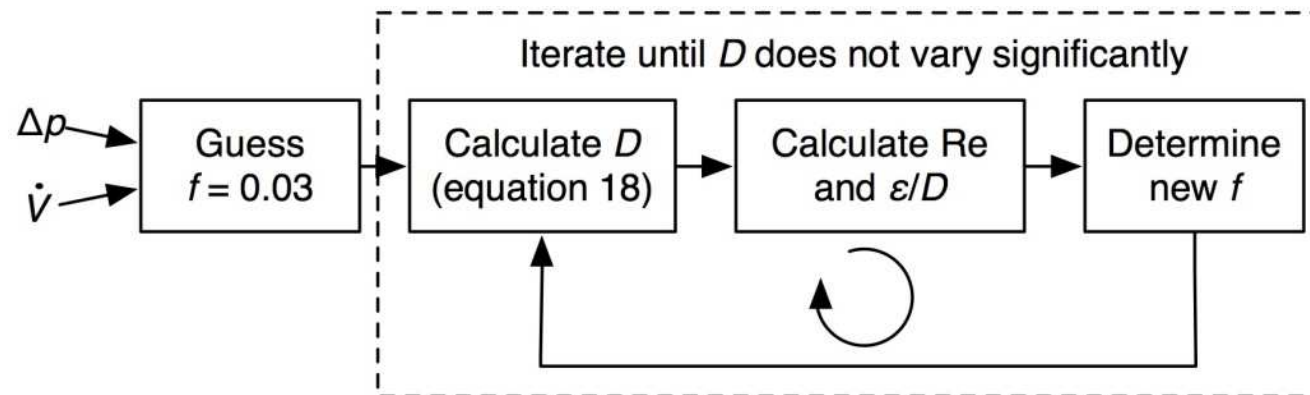
$$\Delta p = \frac{fL}{D} \frac{1}{2} \rho c^2 \rightarrow c = \sqrt{\frac{2\Delta p D}{\rho f L}}$$

Type 3 Problem

- Given:
 - Δp and \dot{V}
- Need to find D
 - We can calculate neither Re nor ϵ/D
 - Assume $f = 0.03$ (middle of Moody)
 - Check solution and iterate if necessary

Type 3 Problem

- Flow chart



$$\Delta p = \frac{fL}{D^5} \frac{8\rho}{\pi^2} \dot{V}^2 \rightarrow D = \sqrt[5]{\frac{fL}{\Delta p} \frac{8\rho \dot{V}^2}{\pi^2}}$$

Example

- Water flows through a 150 mm diameter pipe for which the relative roughness, ε/D is 0.0002 at a rate of 0.1 m³/s. Calculate the pressure drop over a 100 m length of pipe. Take $\mu = 0.001$ kg/ms.

Example

- Water flows through a 150 mm diameter pipe for which the relative roughness, ε/D is 0.0002 at a rate of 0.1 m³/s. **Calculate the pressure drop** over a 100 m length of pipe. Take $\mu = 0.001$ kg/ms.

–MUST BE TYPE 1 PROBLEM!

- On Visualiser

Today's Lecture

- Turbulent flow
- Experimental analysis used to determine a 'friction factor', denoted by f
- Use Reynolds number and Relative Roughness to determine f from Moody Chart

Today's Lecture

- Three types of problems:

– Type 1: use standard equation:

$$\Delta p = \frac{fL}{D} \frac{1}{2} \rho c^2$$

– Type 2: assume full turbulence then iterate to find c , and hence flow rate:

$$\Delta p = \frac{fL}{D} \frac{1}{2} \rho c^2 \rightarrow c = \sqrt{\frac{2\Delta p D}{\rho f L}}$$

– Type 3: assume $f = 0.03$, then iterate to find D

$$\Delta p = \frac{fL}{D^5} \frac{8\rho}{\pi^2} \dot{V}^2 \rightarrow D = \sqrt[5]{\frac{fL}{\Delta p} \frac{8\rho \dot{V}^2}{\pi^2}}$$